

What is claimed:

1. Hydrocracking catalyst composition which comprises an optional metal hydrogenation component supported on a carrier comprising a zeolite of the faujasite structure having a unit cell size in the range of from 24.10 to 24.40 Å, a bulk silica to alumina ratio (SAR) above about 12, and a surface area of at least about 850 m<sup>2</sup>/g as measured by the BET method and ATSM D 4365-95 with nitrogen adsorption at a p/po value of 0.03.
2. A composition as claimed in claim 1, wherein the zeolite has a unit cell size in the range of from 24.14 to 24.38 Å.
3. A composition as claimed in claim 1, wherein the zeolite has a SAR in the range of from about 20 to about 100.
4. A composition as claimed in claim 1, wherein the zeolite has a surface area of at least about 890 m<sup>2</sup>/g.
5. A composition as claimed in claim 1, wherein the zeolite has a micropore volume of at least about 0.28 ml/g.
6. A composition as claimed in claim 1, which further comprises a second zeolite.
7. A composition as claimed in claim 6, which further comprises in the range of from 1 to 5 %by weight of zeolite beta, basis total carrier.
8. A composition as claimed in claim 1, which further comprises a binder.
9. Hydrocracking catalyst composition which comprises an optional metal hydrogenation component supported on a carrier comprising a zeolite of the faujasite structure obtainable by a process which comprises
  - a) hydrothermally treating a zeolite of the faujasite structure having a silica to alumina molar ratio in the range of from about 4.5 to about 6.5, and an alkali content of less than about 1.5 %wt; at

a temperature in the range of from 600°C to 800°C, and at a partial pressure of steam in the range of from about 0.2 to about 1 atmosphere for a time effective to produce an intermediate zeolite having a unit cell size of from 24.30 to 24.45 Å;

b) contacting the intermediate zeolite with an acidified solution comprising an acid and optionally an ammonium salt under conditions effective to produce a high surface area zeolite having a unit cell size in the range of from 24.10 to 24.40 Å, a molar silica to alumina ratio of greater than about 12 and a surface area of greater than about 850 m<sup>2</sup>/g thereby producing the high surface area zeolite; and

c) recovering the high surface area zeolite.

10. A process for the conversion of a hydrocarbonaceous feedstock into lower boiling materials, which comprises contacting the feedstock with hydrogen at elevated temperature and pressure in the presence of a hydrocracking catalyst composition which comprises an optional metal hydrogenation component supported on a carrier comprising a zeolite of the faujasite structure having a unit cell size in the range of from 24.10 to 24.40 Å, a bulk silica to alumina ratio (SAR) above about 12, and a surface area of at least about 850 m<sup>2</sup>/g as measured by the BET method and ATSM D 4365-95 with nitrogen adsorption at a p/po value of 0.03.

11. A process as claimed in claim 10, which is carried out at a temperature in the range of from 250 to 500°C and a total pressure in the range of from 3 x 10<sup>6</sup> to 3 x 10<sup>7</sup> Pa.